Run4Life project. Current results and exploitation pathways



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17th December 2020, ULTIMATE Meeting on Nutrient Recovery

The Run4Life project receives funding from the EU Horizon 2020 Research and Innovation programme, under G.A. No 730285.





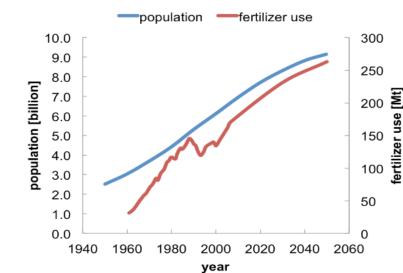
Context

- Global demand for food ↑
- Global demand for fertilisers Λ
- Phosphorus: not renewable, localised reserves
- Nitrogen: "Fertilizer from air" but highly energy demanding

Nutrients in wastewater (WW)

A potential pollutant – and important resource currently not exploited in the conventional, centralised and linear approach based in the old concept of Cloaca Maxima





world population and fertilizer use



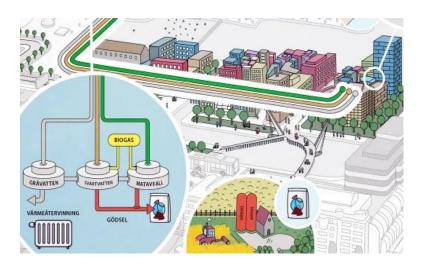


Horizon 2020, GA 730285.

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Run4Life: decentralised resource recovery at the source

- 1. Separation at source
 - Black water (BW), kitchen waste (KW) and grey water (GW)
- 2. Technological innovations and new business models.
- 3. Break barriers to implementation: market uptake, and social and legal acceptance







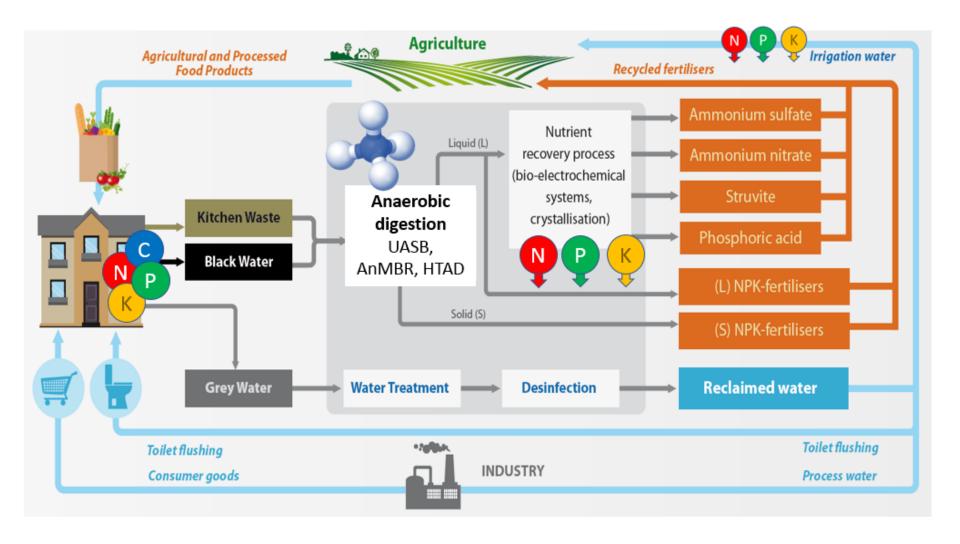
















Nieuwe Dokken - Ghent, Belgium (1200 p.e.)





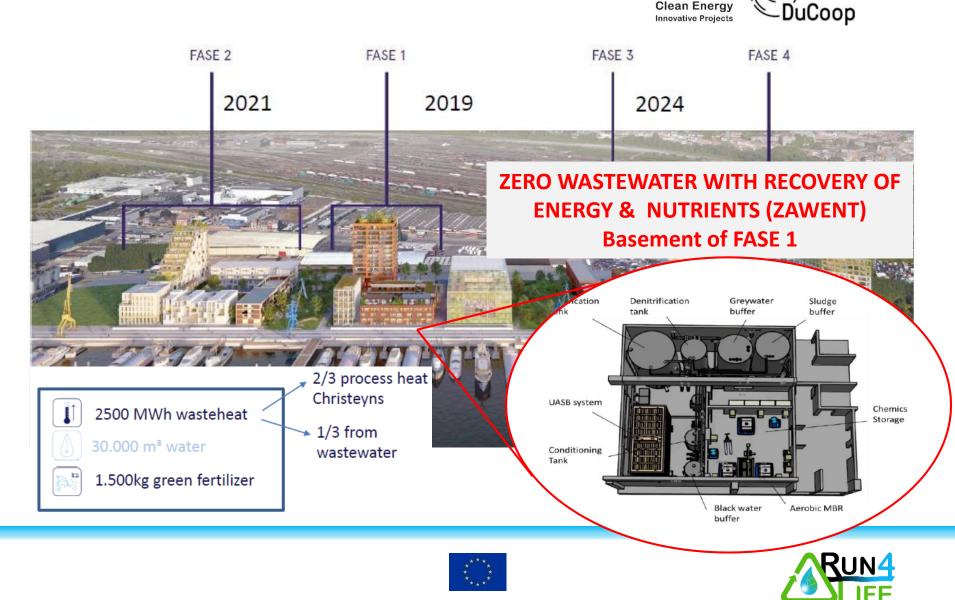


>400 Housing units+ City complex (schools, sports infrastructure etc.)





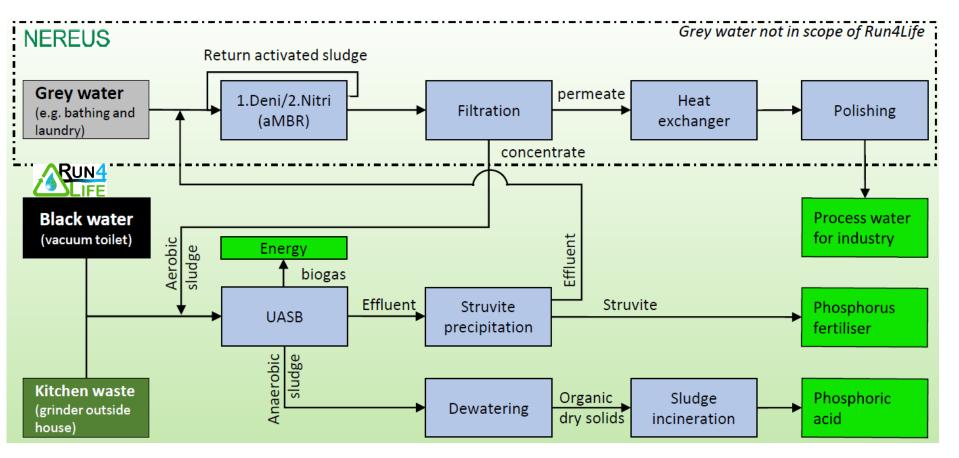
Nieuwe Dokken - Ghent, Belgium (1200 p.e.)



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Nieuwe Dokken - Ghent, Belgium (1200 p.e.)



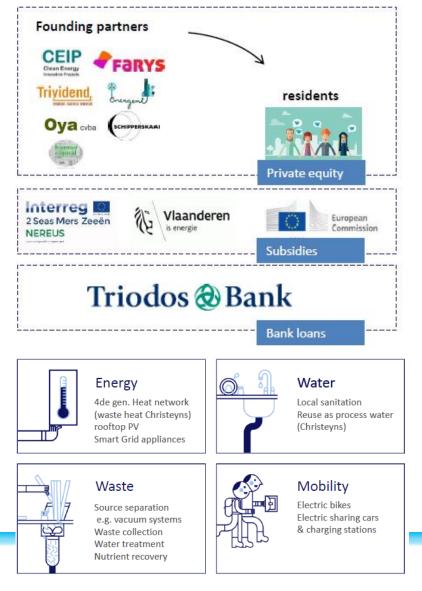






Exploitation: Cooperative business model

Nieuwe Dokken - Ghent, Belgium (1200 p.e.)



How & why a cooperative legal entity?

- > **Cooperation** with citizen participation allow for:
 - Flexible capital
 - Legal limit of 6% IRR
 - Securing fair price setting





- Financial stimulus for end users (correct use of the systems)
- Governance participation by inhabitants
 - Representation in Board and General Assembly
 - Voting right in General Assembly
 - Strong involvement / ambassadors

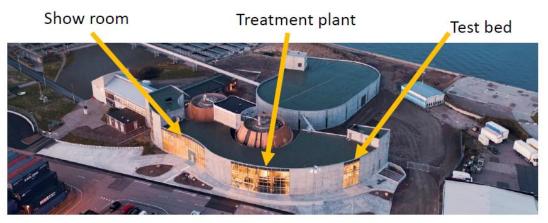




Oceanhamnen (H+) - Helsingborg, Sweden (1800 p.e.) 🌏 🦳

- Innovative waste and wastewater management system.
- Around 320 apartments and several office buildings





Local treatment system

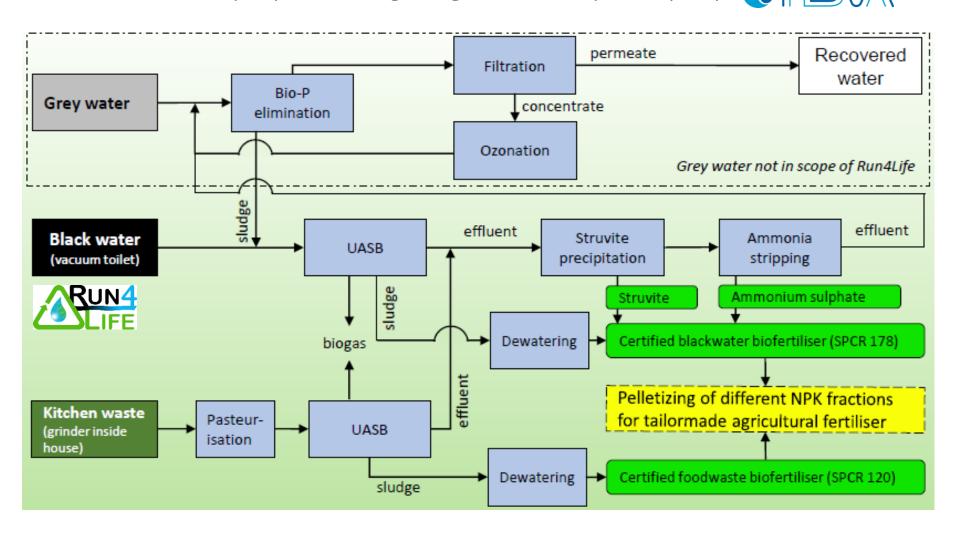
- <u>Reco Lab</u>: Recovery laboratory, test-bed facility
- facility • Educational showroom





Demo sites and technologies

Oceanhamnen (H+) - Helsingborg, Sweden (1800 p.e.) 🜏 🦳







Oceanhamnen (H+) - Helsingborg, Sweden (1800 p.e.) 🜏 🦳

NPK pellet

- **Dewatered food waste sludge** from anaerobic digester (certified as biofertilizer using national certification system)
- Struvite (EU end of waste classified as a product)
- Ammonium sulphate (EU end of waste classified as a product)
- Commercial potassium chloride

Accepted by farmers in Sweden:

- The products are clean (free from heavy metals and organic pollutants)
- **Concentrated** (at least 5% of nitrogen, but preferably up to 20%)
- Spread using conventional equipment



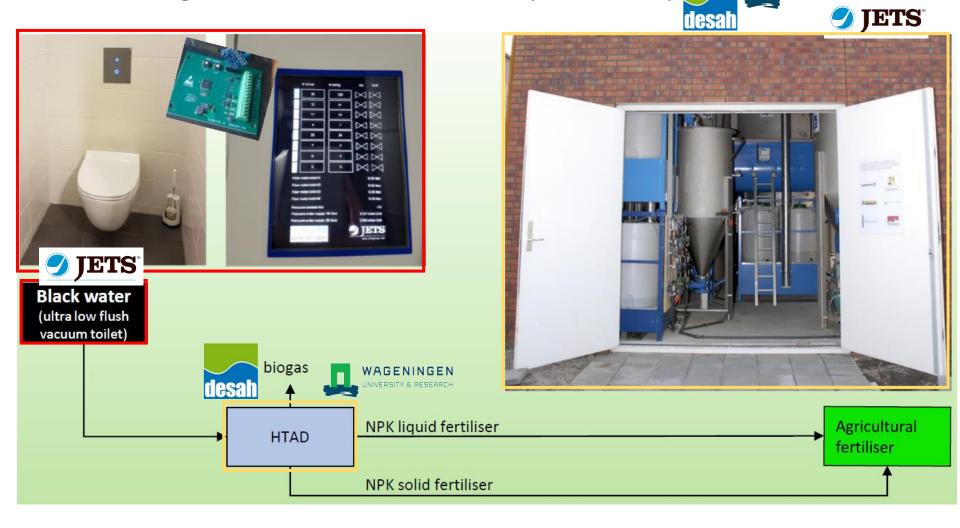






Demo sites and technologies

Lemmerweg - Sneek, the Netherlands (32 houses)







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Innovations: ULF Toilets

- •Normal (gravity sewer) toilets: 4-9 L/flush
- •Conventional vacuum toilets: 0.8-1.5 L/flush
- •ULF vacuum toilets: 0.4-0.7 L/Flush



Benefits

-notable water savings
-smaller piping dimensions
-highly concentrated blackwater

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> 40 g COD/L





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Innovations: (H)TAD

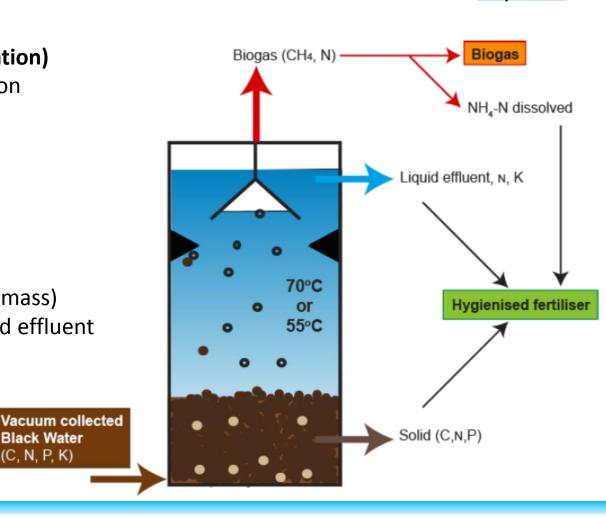
One step for 3 processes (innovation)

- Treatment and biogas production
- Fertiliser production
- Hygienisation

2 main fertiliser streams:

- liquid effluent ٠
- sludge ٠

Most P ends up in the sludge (biomass) Most N and K ends up in the liquid effluent



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Black Water C, N, P, K)



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(H)TAD reactor performance:

Parameter	Unit	Reference 35 °C	Desah 70 °C	Desah 60 °C	Desah 55 °C (ongoing)
HRT	d	11 ± 1.0	14.9 ± 5.0	10.9 ± 1.0	
OLR	gCOD/L/d	0.7 ± 0.1	1.72 ± 0.39	3.5 ± 1.1	
COD in	gCOD/L	10.1 ± 1.8	23.7 ± 2.0	41.7 ± 9.3	Ongoing
COD _T Removal	%	79.1 \pm 4.9	42.2 \pm 14.8	56.5 \pm 17.9	
Methanization	% of COD _{rem}	87.3 \pm 16.4	41.4 \pm 12.3	51.9 \pm 17.6	

- COD removal and methanization increase with decreasing T
- The balance between hygenisation and methane production seems to be around 55°C. (up to 80 % methanization at lab scale).





(H)TAD reactor performance:

Fertiliser Production

	Reference		Run4Life	
	Influent	Effluent	Influent	Effluent
	(35°C)	(35°C)	(60°C)	(60°C)
Total N (g/L)	1.4	1.3	3.8	2.9
NH4-N (g/L)	0.8	1.1	1.5	1.8
Total P (mg/L)	120	96	960	340
PO4-P (mg/L)	101	89	420	164
CARBA (CFU)	0.9	0.03	Not Detected	Not Detected
TBX E.coli (CFU)	5.9	3.6	5.5	Not Detected
ESBL (CFU)	3.9	1.2	3.9	Not Detected





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Full scale installations for decentralised sanitation and resource recovery

Niche market cases:

- New build districts
- High rise buildings
- Sustainable resorts
- Areas with no sewer connection / no capacity for increased sewage flow
- ULF Toilet useful if technology downstream take profit from the ultra concentration of blackwater → Recovery of energy/nutrients





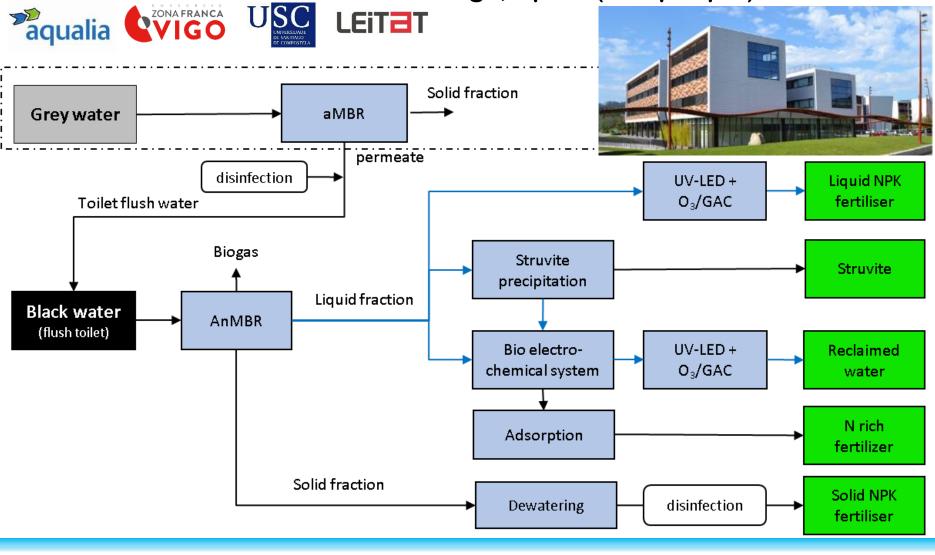
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Demo sites and technologies

Porto do Molle Business Centre - Vigo, Spain (250 people)







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AnMBR treating BW at room temperatura (25 °C).

Flow: $0.8-1.5 \text{ m}^3/\text{d}$ Stable operation:8-10 LMHCOD BW inlet: $1425 \pm 823 \text{ mg/L}$ COD removal:94 %

Steady state biogas production $\approx 0.25 \text{ m}^3/\text{d}$ Methane $\approx 73\%$.



Parameter	Blackwater	Treated water	
Total P (mg/L)	20 ± 10	17 ± 5	
N-NH ₄ ⁺ (mg/L)	115 ± 40	130 ± 45	
Total N (mg/L)	190 ± 70	195 ± 90	
Potassium (mg/L)	120 ± 30	110 ± 30	
рН	7.3 ± 0.3	7.15 ± 0.15	
Alcalinity (mg IC/L)	133 ± 47	117 ± 30	

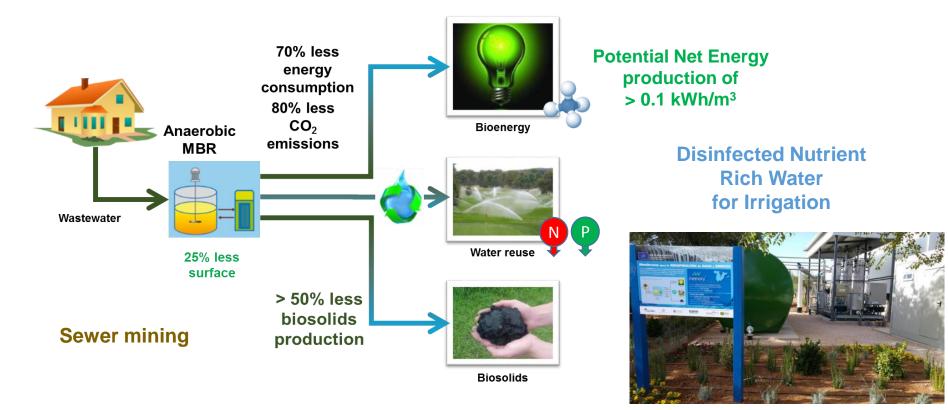




Exploitation

Anaerobic Membrane Bioreactor AnMBR

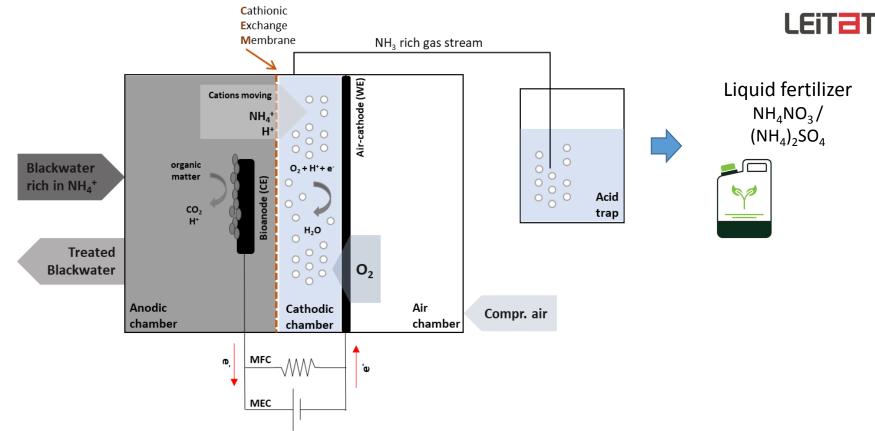








Innovations: Nitrogen recovery with BioElectrochemical Systems (BES)



Operating as MEC in a 5 d batch

- Recovering up to 61% of initial N present in BW (1 g N/L)
- Rate of 12.8 g N/m²/d





Innovations: Nitrogen recovery with BioElectrochemical Systems (BES)

	■N-NH ₄ ⁺ removal ■N-	recov	50% N very in the trap as liquid zer
	Reference MEC in literature	Run4Life MEC system	
Applied potential (V)	0.6-2.12 ^{1,2}	0.2	
Current density (A/m ²)	1.89-30 ^{1,2}	2.78	
N-NH₄ ⁺ removal efficiency (%)	34.3-51 ¹	81	
N-NH₄ ⁺ recovery efficiency (%)	79-94 ²	60	
Energy consumption	6.04-20.5 kWh per kg of nitrogen removed ^{3,4}	 1.61 kWh per kg of nitrog removed⁴ 2.24 kWh per kg of nitrog recovered⁴ 	>50% reduction





Pot and field fertilizer tests









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